

Booklet No.:

CH - 16

Chemical Engineering

| Duration of Test: 2 Hours | | Max. Marks: 120 |
|----------------------------|-----------------|------------------------------|
| | Hall Ticket No. | |
| Name of the Candidate : | | |
| Date of Examination: | OMR An | swer Sheet No.: |
| Signature of the Candidate | | Signature of the Invigilator |

INSTRUCTIONS

- 1. This Question Booklet consists of **120** multiple choice objective type questions to be answered in **120** minutes.
- 2. Every question in this booklet has 4 choices marked (A), (B), (C) and (D) for its answer.
- 3. Each question carries **one** mark. There are no negative marks for wrong answers.
- 4. This Booklet consists of **16** pages. Any discrepancy or any defect is found, the same may be informed to the Invigilator for replacement of Booklet.
- 5. Answer all the questions on the OMR Answer Sheet using Blue/Black ball point pen only.
- Before answering the questions on the OMR Answer Sheet, please read the instructions printed on the OMR sheet carefully.
- 7. OMR Answer Sheet should be handed over to the Invigilator before leaving the Examination Hall.
- 8. Calculators, Pagers, Mobile Phones, etc., are not allowed into the Examination Hall.
- 9. No part of the Booklet should be detached under any circumstances.
- 10. The seal of the Booklet should be opened only after signal/bell is given.

CH-16-A





CHEMICAL ENGINEERING (CH)

| | | 8 | -6 | 2 | |
|----|---------------------------------|----|----|------------|---|
| 1. | If the eigen values of a matrix | -6 | 7 | - 4 | are 0 and 3 then the third eigen value is |
| | NOSON | 2 | -4 | 3 | |

(A) 1

(B) 3

(C) 0

(D) 15

2. The rank of the matrix
$$\begin{bmatrix} 3 & 1 & 4 \\ 0 & 5 & 8 \\ -3 & 4 & 4 \end{bmatrix}$$
 is

(A) 1

(B) 3

(C) 2

 $(D) \quad 0$

3. The gradient of a function
$$\phi(x, y, z) = xy + yz + zx$$
 at the point $(1, 2, 0)$ is

2i + j + 2k(A)

(B) i - 2j + k

(C) i + 2j + 2k

(D) 2i+k

4. If
$$\phi_1 = 0$$
 and $\phi_2 = 0$ are scalar functions then the angle between ϕ_1 and ϕ_2 is

- (A) $\cos^{-1} \frac{\nabla \phi_1 \nabla \phi_2}{|\nabla \phi_1| . |\nabla \phi_2|}$ (B) $\tan^{-1} \frac{\nabla \phi_1 + \nabla \phi_2}{|\nabla \phi_1| . |\nabla \phi_2|}$ (C) $\nabla \phi_1 . \nabla \phi_2$ (D) $\sin^{-1} \nabla \phi_1 . \nabla \phi_2$

(C) $\nabla \phi_1 \cdot \nabla \phi_2$

(D) $\sin^{-1}\nabla\phi_1.\nabla\phi_2$

5. The value of
$$\oint_C (x^2 - y^2 + 2ixy)dz$$
, where C is the contour $|z| = 1$ is

 $(A) \quad 0$

(C) π

(D) $-\pi i$

6. The integrating factor of the differential equation
$$\frac{dx}{dy} + \frac{3}{y}x = \frac{1}{y^2}$$

(A) $e^{\log y}$

(B) e^{y^3}

(D) y

7. The Laplace transform of
$$\sinh 2x$$
 is

 $(A) \quad \frac{2}{s^2 + 4}$

(B) $\frac{2}{s^2 - 4}$

(C) $\frac{2}{s^2+2}$

(D) $\frac{2}{s^2-2}$



| 8. | If f | $f(x) = x + x^2$ satisfy Lagrange Mean | Value | theorem in [0,2] at c, then |
|-------------|----------------------|--|---------------------|--|
| | (A) | c = 0 | (B) | c = 3 |
| | (C) | c = 1 | (D) | c = 2 |
| | | | | |
| 9. | The | function $f(x, y) = xy + (\frac{1}{x} + \frac{1}{y})$ is m | inimu | m at the point |
| | | (1,1) | | (0,1) |
| | | (1,2) | 25 25 | (0,0) |
| | | | | |
| 10. | If y(| $(x_i) = y_i$, $i = 0, 1, 2, 3$ and h the step size | ze the | n by Simpson $1/3^{\text{rd}}$ rule $\int_{x_0}^{x_3} y(x) dx$ |
| | | - | (B) | $\frac{h}{3} [y_0 + 2y_1 + 2y_2 + y_3]$ |
| | (C) | $\frac{h}{2} \big[y_0 + 4y_1 + 2y_2 + y_3 \big]$ | (D) | $\frac{h}{3} [y_0 + 4y_1 + 2y_2 + y_3]$ |
| 11. | Acco | ording to Hydrostatic equilibrium, th | ne nres | sure in a static fluid depends on |
| 11. | (A) | Location in cross-section | 100000 | Location in cross-section and elevation |
| | (C) | Elevation only | (D) | None of the above |
| | | | | Acc. 2004.002 |
| 12. | | term that is not a part of Bernoulli's | | |
| | (A) (C) | Enthalpy Elevation | (B) (D) | Pressure Velocity |
| | (- / | | X - X | |
| 13. | The 1 | Transport to the transport of the transp | | wn by a U tube manometer is a function of |
| | (A) | Height of process fluid in the left a | | |
| | (B) (C) | Height of process fluid in the right Height of manometric fluid in left | | |
| | (D) | Height difference of manometric fl | | both arms. |
| | | 3. | | |
| 14. | 20 M 1 A W 20 M 20 M | Pseudo-plastic fluid, which is true | | |
| | (A) | viscosity decreases with time | (B) | viscosity decreases with time |
| | (C) | viscosity increases with shear rate | (D) | viscosity decreases with shear rate |
| 15. | For a | laminar flow of a fluid in a tube (N | $I_{Re}=10$ | 00), the fanning friction factor is |
| | (A) | 0.16 | (B) | 0.016 |
| | (C) | 1.6 | (D) | 16 |
| 16. | The a | dimensions of dynamic viscosity are | Y | |
| 100 | | ML ⁻¹ T ⁻¹ | | $M^{-1}L^{-1}T^{-1}$ |
| | (C) | ML^2T^{-1} | (D) | MLT ⁻² |
| Set - | A | | 3 | СН |
| 1000 1000 L | | | | |
| | | | | |



| 17. | The | frictional loss in | an unseparated bou | ındary | layer is called | 95 | | |
|-----------------|--------|--|--|--------|-----------------------|----------------|---------------|------|
| | (A) | Form Friction | | (B) | Pressure Frict | ion | | |
| | (C) | Dynamic Friction | on | (D) | Skin Friction | | | |
| | | | | | | | | |
| 18. | The | pressure drop in a | a packed bed | | | | | |
| | (A) | Navier Stokes e | quation | (B) | Euler's Equat | ion | | |
| | (C) | Ergun Equation | | (D) | Bernoulli's ed | quatio | n | |
| 19. | The | velocity profile o | f a laminar flow of | fa Ne | aztonian fluid i | n a tuk | ne is | |
| *** | (A) | | B) Parabolic | (C) | Hyperbolic 1 | (D) | Sinusoidal | |
| | (A) | Linear (| b) Tarabone | (0) | rryperbone | (1) | Smusoidai | |
| 20. | Тоа | void cavitation in | a pump, the main | princ | iple to be appli | ed is | | |
| | (A) | Maintain NPSH | | (B) | Do Priming | | | |
| | (C) | Do Cleaning | | (D) | Apply lubrica | int | | |
| 21 | YY | f.1f | | 4 | 7 | -11 | . 1 (6 2) | |
| 21. | | | centrifugal pump i | | | ener s | speed in as | |
| | (A) | n | | (B) | n^2 | | | |
| | (C) | n^3 | | (D) | n | | | |
| 22. | The | drag coefficient f | or the flow a past s | sphere | in stokes law | regimo | e is given by | |
| | (A) | 16/N _{Rc,p} | 0 (0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 0 | (B) | N _{Re,p} /16 | 0 | | |
| | (C) | $24/N_{Rc,p}$ | | (D) | N _{Re,p} /24 | | | |
| 4929 | 25-042 | 80000 60 St 50 1001 | | | | 1000 | 500 BI 6 | 8 24 |
| 23. | | skin friction loss along the flow of 10 m of the pipe (100 mm diameter) at a velocity 0m/s is (given fanning friction factor is 0.001) | | | | | | |
| | (A) | 20 J/kg | | (B) | 5 J/kg | | | |
| | (C) | 40 J/kg | | (D) | 10 J/kg | | | |
| 2 8 | 10 | 21 12 12 13 | 91 100 s | 3 | | | | |
| 24. | Amo | ong the flow device | ces, the linear one | is | | | | |
| | (A) | Venturimeter | | (B) | Nozzle meter | | | |
| | (C) | Orificemeter | | (D) | Rotameter | | | |
| 25. | For a | an ideal screen | | | | | | |
| 20007-0720-0500 | (A) | | overflow is slightly | large | r than the large | est in t | he underflow | |
| | (B) | | overflow is very m | - | - | | | |
| | (C) | | overflow is slightly | | | 01 10 | | |
| | (D) | | overflow is sugarry | | | | | |
| Set - | A | | 4 - .0 | 4 | | U- T (1 | | СН |
| 10000 10000 | | | | | | | | |



| 26. | The | collection efficiency in a cyclone in | crease | es with | |
|--------|-------|---|--------------|--|----|
| | (A) | decrease in particle density | (B) | decrease in viscosity of gas | |
| | (C) | increase in viscosity of gas | (D) | increase in temperature of gas | |
| 27. | For a | a particle dropped inside a stagnant | fluid, | the force that shall not act is | |
| | (A) | weight of particle | (B) | drag force | |
| | (C) | centrifugal force | (D) | buoyant force | |
| 28. | Acco | ording to which law of crushing, the | work | required is constant for same size ratio | ? |
| | (A) | Rittingers Law | (B) | Bonds Law | |
| | (C) | Kicks Law | (D) | Newton's Law | |
| 29. | Тоа | void centrifuging in a ball mill, the | operat | ting speed should be | |
| | (A) | Slightly less than critical speed | ** | | |
| | (B) | Very much less than critical speed | | | |
| | (C) | Slightly greater than critical speed | | | |
| | (D) | Very much larger than critical spec | | | |
| 30. | The | fluid that shows time dependent rhe | eology | ı is | |
| | (A) | Thixotropic Fluid | (B) | Pseudo plastic Fluid | |
| | (C) | Dilatant Fluid | (D) | Binghamplastic Fluid | |
| | 2000 | | | | |
| 31. | The | mode of heat transfer in which Four | riers L | aw is applicable is | |
| | (A) | Conduction | (B) | Forced Convection | |
| | (C) | Radiation | (D) | Free Convection | |
| 32. | The | units of heat transfer coefficient is | | | |
| | (A) | W/m.K | (B) | W/m^2K | |
| | (C) | J/m.K | (D) | J/m^2K | |
| 33. | In a | pool boiling phenomenon, the prefe | erred r | regime is | |
| | (A) | Transition Boiling | (B) | Radiative Boiling | |
| | (C) | Film Boiling | (D) | Nucleate Boiling | |
| 34. | | convective heat flux in SI units thro s (SI) with a temperature difference | 352 Sycamore | medium of heat transfer coefficient 100°C is |) |
| | (A) | 5000 | (B) | 2 | |
| | (C) | 0.5 | (D) | 500 | |
| Set -[| A | | 5 | | CH |



| 35. | | e dimensionless group that gives the ratio of thermal to hydrodynamic boundary layer cknesses is | | | | |
|-------------|--|--|-------|--|------|--|
| | (A) | Nusselt Number | (B) | Prandtl Number | | |
| | (C) | Reynolds Number | (D) | Grashoff Number | | |
| | | | | | | |
| 36. | The | emissivity of a black body is | | | | |
| | (A) | 1 | (B) | >1 | | |
| | (C) | 0 | (D) | <1 | | |
| 37. | Acco | ording to Stefan Boltzmann law, the | emiss | sive power of black body is proportional | l to | |
| | (A) | T | (B) | T^2 | | |
| | (C) | T^3 | (D) | T^4 , where T is absolute temperature | | |
| 10000 10400 | 720242 IV | | 20 | | | |
| 38. | | economy of an evaporator is defined | l as | | | |
| | (A) | Steam consumed/hr | | | | |
| | (B) | Water evaporated/hr | | | | |
| | (C) | Steam consumed/water evaporated | | | | |
| | (D) | Water evaporated/steam consumed | 1 | | | |
| 39. | In ge | eneral, the major resistance in film t | уре с | ondensation is | | |
| | (A) | Liquid side | (B) | Vapor side | | |
| | (C) | Wall side | (D) | Fouling | | |
| 40 | TI. | | 1 | | | |
| 40. | 11120000000000000000000000000000000000 | product of Grashoff and Reynolds n | | | | |
| | (A) | Prandtl Number | (B) | Peclet Number Nusselt Number | | |
| | (C) | Rayleigh's Number | (D) | Nusselt Number | | |
| 41. | Ove | rall thermal resistance in a heat exch | anger | is proportional to | | |
| | (A) | Overall heat transfer coefficient | | | | |
| | (B) | Reciprocal of overall heat transfer | coeff | icient | | |
| | (C) | Overall temperature drop | | | | |
| | (D) | Temperature difference across the | wall | | | |
| 42. | In a | closed system, which is true? | | | | |
| 12. | (A) | Only energy exchange | | | | |
| | (B) | Only mass exchange | | | | |
| | 1000000000 | Neither mass nor energy exchange | | | | |
| | (D) | Both mass and energy exchange | | | | |
| Set - | A | constituer settled | 6 | | СН | |



| 43. | | | f seco | nd law, if in a heat engine heat taken from |
|-------|-------|--|----------------|--|
| | (A) | ce is 100 units, then Heat delivered to sink should be 1 | 00 un | ite |
| | | Work done should be 100 units | OO un | 11.5 |
| | (B) | | | |
| | (C) | Work done cannot be 100 units | ΛΛ | 1 200 |
| | (D) | Heat delivered to sink cannot be 1 | 00 un | its |
| 44. | | | oes 40 | J work by taking 100 J heat, then the change |
| | | internal energy is | 12. | 51 C |
| | (A) | 140 J | (B) | -60 J |
| | (C) | -140 J | (D) | +60 J |
| 45. | An i | sentropic process is | | |
| | (A) | Reversible | (B) | Adiabatic |
| | (C) | Reversible Adiabatic | (D) | Reversible Isothermal |
| 46. | In a | compressible cake | | |
| | (A) | Cake resistance is function of time | 2 . | |
| | (B) | Cake resistance is function of pos | | nd time. |
| | (C) | Cake resistance is not function of | | |
| | (D) | Cake resistance is not function of | | on. |
| 47. | Parti | al molar Gibbs free energy is also o | ralled | |
| | (A) | N20 N N | (B) | Fugacity |
| | (C) | Chemical Potential | (D) | Entropy |
| | (0) | Chemical Fotolicial | (12) | Бинору |
| 48. | | and the analysis of the contract of the contra | efine tl | ne system of water and toluene (immiscible) |
| | | ontact with its vapors is | (D) | 2 |
| | (A) | | (B) | 2 |
| | (C) | 3 | (D) | 4 |
| 49. | | | 3.2 | essor (neglecting kinetic and potential energy |
| | | ges), the work done on it is equal to | | 1.00 |
| | (A) | | (B) | ΔU |
| | (C) | ΔΗ | (D) | ΔS |
| 50. | Whi | ch is true according to principle of | increas | se of entropy? |
| | (A) | ΔS system>0 | (B) | ΔS surroundings>0 |
| | (C) | ΔS system>=0 | (D) | ΔS universe>=0 |
| 51. | Whi | ch is not a VLE model? | | |
| | (A) | Raoults Law | (B) | Hess Law |
| | (C) | Modified Raoults Law | (D) | Henry's Law |
| Set - | A | | 7 | СН |
| W 75 | | | | |



| 52. | Whi | ch of the combinations indicate Bu | bble p | oint calculation? |
|-------------|---------------|--|----------|--|
| | i. | Calculate yi and T given x and P | | |
| | ii. | Calculate xi and T given y and P | | |
| | iii. | Calculate yi and P given x and T | | |
| | iv. | Calculate xi and P given y and T | | |
| | (A) | i and ii | (B) | ii and iii |
| | (C) | i and iii | (D) | i and iv |
| | | | | |
| 53. | Enth | alpy change of mixing ideal gases v | would | be |
| | (A) | 0 | (B) | Positive |
| | (C) | Negative | (D) | Can't say |
| 54. | 200 | nal energy of a two phase mixtur kJ/kg and 1200 kJ/kg for saturated b 1400 kJ/kg | | 40% quality is (internal energy values are and vapor respectively). 700 kJ/kg |
| | (A) | 000 CONTROL OF CONTROL | | |
| | (C) | 600 kJ/kg | (D) | 1000 kJ/kg |
| 55. | Whi | ch thermodynamic function is called | 1 as G | enerating function ? |
| | (A) | 3 DESCRIPTION OF A STATE OF STATE O | (B) | |
| | (C) | Entropy | (D) | Gibbs Free Energy |
| | 161 161 | 5(0.7) | 13 61 | |
| 56. | gase | | | $g(g) \rightarrow CO_2(g) + H_2(g)$, (all species are ideal bar pressure, the extent at 20 bar pressure |
| | (A) | 0.5 | (B) | 1.0 |
| | (C) | 0.25 | (D) | 0.75 |
| 57 | XX/L: | ah ia mat tuna maganding hymnas atma | ? | |
| 57. | 20100 | ch is not true regarding bypass strea | 1111 7 | |
| | (A) | Passes through all stages | ion | |
| | (B) (C) | Affects the final product composit | .IOII | |
| | (D) | Skips one or more stages Affects the component material ba | lance | |
| | (D) | Affects the component material ba | nance. | 5 |
| 58. | solve 10 k | ent (M.W=20 kg/kmol). The solubi | ility at | oles of solute (M W=50 kg/kmol) per kg of 100 °C is 10 moles of solute/kg solvent. If °C, then the weight of the additional solute |
| | (A) | 0.25 kg | (B) | 1 kg |
| | (C) | 2 kg | (D) | 3.34 kg |
| Set - | A | | 8 | СН |
| 1000 (050 L | | | 16 | |



| 59. | 927 | | | | air (21% O_2 and 79% N_2) in mole percent on N_2 -87.1%. Then the mole ratio of CH ₄ to O_2 |
|-----------|------------|--|--------------------|------------|---|
| | | feed stream is | | | |
| | | 1.05 | (I | 3) | 0.6 |
| | (C) | 0.51 | |)) | 0.45 |
| 60. | | | | | CO ₂ , if the standard heats of formation of CO |
| | | | å 1851 192 | 2890 | dard heat of the reaction is |
| | (A) (C) | H_1+H_2 - H_1-H_2 | | 3))) | H_1-H_2 H_2-H_1 |
| | (C) | -111-112 | (1 |) | 112-11 |
| 61. | Whic | h among the following | ng is not a steady | sta | ate flow reactor? |
| | (A) | CSTR | (1 | 3) | Plug Flow Reactor |
| | (C) | Batch Reactor | (I | D) | Tubular Reactor |
| 62. | The u | units of a first order ra | ate constant | | |
| · | | Sec ⁻¹ | | 3) | mol lit ⁻¹ sec ⁻¹ |
| | | lit.mol ⁻¹ sec ⁻¹ | | | lit ⁻¹ mol ⁻¹ sec ⁻¹ |
| 63. | 0.000 | | 250 | 6.0 | oducts, a plot of 1/C _A vs time gives a straight |
| | | of intercept and slope | 0.5 | | outen, a protot it ex to time gives a stranger |
| | (A) | CAO and k | (I | 3) | 1/C _{AO} ; 1/k |
| | (C) | $1/C_{\Lambda O}$, k | (I | O) | C_{AO} , $1/k$ |
| 64. | | PFR of volume 200 li :10 mol/lit, the space | | v ra | ate is 100 mol/hr at an initial concentration of |
| | (A) | 10 hr | 9203 | 3) | 20 hr |
| | (C) | 30 hr | <u> </u> | O) | 40 hr |
| 65. | For th | he reaction $A \rightarrow 5R$, | the fractional ch | ans | ge in volume ε is |
| | (A) | | | 3) | · 10 |
| | (C) | 4 | |)) | |
| | 100 m | | 28 | <u>(1)</u> | |
| 66. | | constant density systemated and final concentrated and final concent | | der | the plot of $-1/r_{\Lambda}$ vs C_{Λ} for a PFR between |
| | (A) | $T/C_{\Lambda O}$ | (I | 3) | T |
| | (C) | V/F _{AO} | (I |) | 1/T |
| 67. | N PF | Rs in series of with a | a total volume of | V | gives the same conversion as a single PFR of |
| | volur | ne | | | |
| | (A) | NV | (I | 3) | V/N |
| | (C) | V | (I |)) | 2NV |
| Set - | A | | 9 | | СН |
| 1993 1994 | | | | | Too. |



| 68. | In an ideal CSTR, the concentration | of specie | s inside the reactor is | |
|-------|--|-------------------------|--|-----|
| | (A) Same as Inlet | (B) | Same as Exit | |
| | (C) Not same as Exit | (D) | Can't say | |
| 69. | The half-life of n th order reaction in a | a batch re | actor depends on | |
| | (A) Rate constant | (B) | Order of reaction | |
| | (C) Initial concentration | (D) | All of the above | |
| 70. | For solid catalyzed reactions, Thiele | modulus | is defined as | |
| | (A) diffusion rate/intrinsic reaction | | | |
| | (B) [diffusion rate/intrinsic reaction | n rate] 1/2 | | |
| | (C) intrinsic reaction rate/diffusion | | | |
| | (D) [intrinsic reaction rate/diffusion | on rate] ^{1/2} | | |
| 71. | The units of residence time distributi | on, E is | | |
| | (A) time | (B) | No Units | |
| | (C) time ⁻¹ | (D) | time ⁻² | |
| 72. | The slow reactions in gas/porous cata | alyst syst | ems are influenced by | |
| | (A) Pore diffusion | (B) | Surface kinetics | |
| | (C) Film diffusion | (D) | Particle ΔT | |
| 73. | The reactor that suits the most for stu | adying th | e kinetics of solid catalyzed reactions is | |
| | (A) Batch reactor | (B) | Differential reactor | |
| | (C) Packed bed reactor | (D) | Mixed Flow reactor | |
| 74. | The resistance to pore diffusion is gi | ven by | | |
| | (A) Thiele modulus | (B) | Weisz modulus | |
| | (C) Effectiveness factor | (D) | All of the above | |
| 75. | For heterogeneous systems, the excompared to homogeneous system is | | n that comes in the rate expression wh | nen |
| | (A) Mass transfer term | (B) | Concentration term | |
| | (C) Temperature term | (D) | None | |
| 76. | For dilute solutions, diffusivity in liq | uids is p | roportional to | |
| | (A) $T^{3/2}$ | (B) | T | |
| | (C) $T^{1/2}$ | (D) | No effect | |
| | where T is the absolute tempera | ature of se | olution. | |
| Set - | A | 10 | C | H |



| Set -[| A | | 11 | СН |
|--------|---------------------------|---|-----------------------|---|
| 85. | (A) | units of gas hold-up is m ³ m ³ /m ³ | (B) (D) | m ³ /kg kg/m ³ |
| 84. | activities that the co | gas-liquid operation, at very low ga id rains down through the openings Flooding Weeping | | cities, the phenomenon in which much of the tray is Coning Dumping |
| 83. | As rei ii iii iiv (A) (C) | Perflux ratio in distillation is increased. Number of trays become zero. Operating curves coincide with 45 Number of trays becomes infinity. Operating curves deviate most from i and ii ii and iv. | 5° diag | onal |
| 82. | The : (A) (C) | single stage operation among the fo Continuous Rectification Fractionation | ollowir (B) (D) | ng is Differential Distillation Flash Vaporization. |
| 81. | No s (A) (C) | | | value of relative volatility, α is 1.25 2.0 |
| 80. | | | | tes are 1.796x10 ⁻³ kmol/s and 0.01052 kmol/s e is 0.1225, then the absorption factor is 1.366 0.889 |
| 79. | Whice (A) (B) (C) (D) | ch is not the characteristic of an ide Small interfacial area between phat Large interfacial area between phat Chemically inert Structural strength | ases | er packing material in gas-liquid operations? |
| 78. | is (A) (C) | Reynolds Number Prandtl Number | (B) (D) | ransfer to Sherwood number in mass transfer Nusselt Number Grashoff Number |
| | (A) (C) | Surface Stretch theory Film theory | (B) (D) | Surface Renewal theory Penetration theory |
| 77. | The | theory that no stulates the steady sta | te con | centration gradient is |



| (B) moles transferred/(area)(time)(mole fraction) (C) moles transferred/(area)(time)(mass fraction) (D) moles transferred/(area)(time)(mass) 87. In drying, if moisture contained by a substance exerts an equilibrium vapor pressuless than that of the pure liquid at the same temperature is (A) Free Moisture (B) Bound Moisture (C) Unbound Moisture (D) Equilibrium Moisture 88. Which is not recommended for leaching operation? (A) High temperature (B) Low temperature | ure that is |
|--|------------------------|
| (D) moles transferred/(area)(time)(mass) 87. In drying, if moisture contained by a substance exerts an equilibrium vapor pressuless than that of the pure liquid at the same temperature is (A) Free Moisture (B) Bound Moisture (C) Unbound Moisture (D) Equilibrium Moisture 88. Which is not recommended for leaching operation? | ure that is |
| 87. In drying, if moisture contained by a substance exerts an equilibrium vapor pressuless than that of the pure liquid at the same temperature is (A) Free Moisture (B) Bound Moisture (C) Unbound Moisture (D) Equilibrium Moisture 88. Which is not recommended for leaching operation? | ure that is |
| less than that of the pure liquid at the same temperature is (A) Free Moisture (B) Bound Moisture (C) Unbound Moisture (D) Equilibrium Moisture 88. Which is not recommended for leaching operation? | ure that is |
| (C) Unbound Moisture (D) Equilibrium Moisture 88. Which is not recommended for leaching operation? | |
| 88. Which is not recommended for leaching operation? | |
| 200-0000 12-010000 mm | |
| (A) High temperature (B) Low temperature | |
| | |
| (C) High solubility of solute (D) Low liquid viscosity | |
| 89. In the McCabe thiele diagram, if the x coordinate of the point of intersection of of the vapor-liquid equilibrium curve is greater than the x coordinate of the feed p the quality of the feed is | |
| (A) Saturated Vapor (B) Superheated Vapor | |
| (C) Liquid below bubble point (D) Saturated liquid | |
| 90. If in a counter current gas absorption, if the liquid-gas flow rate is increased, ther true? | which is |
| (A) Operating line shifts towards equilibrium curve (B) Operating line shifts away from equilibrium curve | |
| (C) No shift of the operating line | |
| (D) Concentration of absorbed species increases in the exit liquid stream. | |
| 91. Which of the pressure sensors is non-linear? | |
| (A) Liquid column manometer (B) Ring Balance | |
| (C) Strain gauge on diaphragm (D) LVDT type | |
| 92. Which class of temperature measurement systems applies for widest range of tem | perature? |
| (A) Solid Expansion type (B) Resistance type | |
| (C) Thermocouple type (D) Liquid Expansion type | |
| 93. A constant volume gas thermometer works on the principle of | |
| (A) Archimedes principle (B) Boyle's Law | |
| (C) Charles Law (D) Pascal's Law | |
| 94. The generation of emf in thermocouples is explained by | |
| (A) Seebeck effect (B) Ohms Law | |
| (C) Stefan Boltzmann Law (D) Joule Heating effect | |
| Set - A 12 | $\mathbb{C}\mathbb{H}$ |

Which cannot be the unit for mass transfer coefficient?



| | (A) | it does not bend | | | | |
|---|--|--|--------|--|----|--|
| | (B) | it gets twisted | | | | |
| | (C) | it bends with iron on concave side | | | | |
| | (D) | it bends with copper on concave si | | | | |
| 96. | Whi | Which is incorrect regarding the first order response system ? | | | | |
| Which is incorrect regarding the first order response system? (A) $\Delta(\text{Input})=\text{Kp }\Delta(\text{Output})$ | | | | | | |
| | (B) | $\Delta(\text{Output}) = \text{Kp} \Delta(\text{Output})$ $\Delta(\text{Output}) = \text{Kp}$ | | | | |
| | (C) | | | | | |
| | (D) | $\Delta(\text{Output}) = \text{Kp } \Delta(\text{Input}), \text{ where } \text{Kp}$ | is ste | eady state gain. | | |
| 97. | 7. For a first order system, after one time constant, the percent response attained value is | | | | | |
| | (A) | 33.33% | (B) | 63.2% | | |
| | (C) | 75.5% | (D) | 100%. | | |
| 98. | Whic | ch is not true regarding PI control? | | | | |
| | (A) | Order of response decreases | | | | |
| | (B) | Order of response increases | | | | |
| | (C) | Large Kc values produce very sen | sitive | response | | |
| | (D) | As time constant decreases for cor | istant | Kc, response becomes more oscillatory | | |
| 99. The amplitude ratio is defined as | | | | | | |
| | | $K_{p}/[T_{p}^{2}\omega^{2}+1]$ | (B) | $[T_p^2 \omega^2 + 1]/K_p$ $K_p/[T_p^2 \omega^2 + 1]^2$ | | |
| | (C) | $K_p/[T_p^2\omega^2+1]^{1/2}$ | (D) | $K_{\rm p}/[T_{\rm p}^2\omega^2+1]^2$ | | |
| 100. | The | time lag of a first order instrument i | S | | | |
| | (A) | T | (B) | $(1/\omega) \tan^{-1} (\omega T)$ | | |
| | (C) | $(\omega) \tan^{-1} (\omega T)$ | (D) | e^{-T} | | |
| 101. | The | The major drawback of ammonium nitrate as a fertilizer is | | | | |
| | (A) | High Nitrogen content | (B) | Quick acting nitrate | | |
| | (C) | Slow acting ammoniacal nitrogen | (D) | Tendency to cake on storage | | |
| 102. | Whic | ch is incorrect regarding sulfuric aci | id? | | | |
| | (A) | Dibasic acid | (B) | Dehydrating agent | | |
| | (C) | Reducing agent | (D) | Forms hydrates | | |
| 103. | Oleu | ms are | | | | |
| | (A) | | (B) | H ₂ SO ₄ in water | | |
| | (C) | HNO ₃ in water | (D) | NO ₃ in water | | |
| Set -[| A | | 13 | | CH | |
| | | | | | | |

When a strip of iron and copper is heated



| 104. | In the Krast pulping process, the primary material added to the cooking liquor is | | | | |
|-------|---|--------|---------------------------------------|----|--|
| | (A) Na ₂ SO ₄ | (B) | H_2SO_4 | | |
| | (C) NaHSO ₄ | (D) | Lime | | |
| 105. | Sizing is added to paper mainly to | | | | |
| | (A) have desired color | | | | |
| | (B) improve the finish | | | | |
| | (C) increase penetration resistance to | liquid | S | | |
| | (D) to reduce cost | | | | |
| 106. | Which operation is not involved in oil processing? | | | | |
| | (A) Bleaching | (B) | Dehydrogenation | | |
| | (C) Refining | (D) | Deodorization | | |
| 107. | Phosphatic fertilizer is graded based on its | | | | |
| | (A) P content | (B) | PCl ₃ content | | |
| | (C) H ₃ PO ₄ content | (D) | P ₂ O ₅ content | | |
| 108. | Bleaching powder is represented by the formula | | | | |
| | (A) $Ca(ClO_3)_2$ | (B) | CaCl(OCl) | | |
| | (C) Ca(OCl) ₂ | (D) | $Ca(ClO_4)_2$ | | |
| 109. | Soap may be manufactured by | | | | |
| | (A) hydrolysis of tallow | | | | |
| | (B) hydrogenation of vegetable oils | | | | |
| | (C) boiling of vegetable oils/tallow with caustic soda solution | | | | |
| | (D) oxidation of tallow | | | | |
| 110. | For petroleum products, °API is given by | | | | |
| | (A) (131.5/S)-141.5 | (B) | (141.5/S)-131.5 | | |
| | (C) (145/S)-130 | (D) | 141.5-(131.5/S) | | |
| | where S is specific gravity at 60°F/60° | F. | | | |
| 111. | Profitability measure that considers time value of money is | | | | |
| | (A) Net present worth | (B) | Return on investment | | |
| | (C) Payback period | (D) | Net return | | |
| 112. | Which does not come under working capital? | | | | |
| | (A) Raw materials | (B) | Salaries | | |
| | (C) Equipment | (D) | Finished products in stock | | |
| Set - | A | 14 | | CH | |



| | (A) | $i_{eff}=ln(r+1)$ | (B) | $i_{eff}=e^{r}-1$ | | |
|-----------|--|--|------------|---------------------------------|--|--|
| | (C) | $i_{eff}=lnr-1$ | (D) | $i_{eff}=e^{r}$ | | |
| | | | | | | |
| 114. | In a | straight line depreciation method, it | is ass | umed that the value of property | | |
| | (A) | decreases linearly with time | | | | |
| | (B) | decreases exponentially with time | | | | |
| | (C) | decreases logarithmically with tim | e | | | |
| | (D) | remains constant with time | | | | |
| 115. | Droo | ant worth D of future amount of mo | nov E | for discrete discounting is | | |
| 115. | | ent worth P, of future amount of mo P=Fe ^{-rN} | 00000 | F=Pe ^{-rN} | | |
| | (A) | $P=Fe$ $P=F(1+i)^{-N}$ | 70000 | $F=Pe$ $F=P(1+i)^{-N}$ | | |
| | (C) | P=F(1+1) | (D) | $\Gamma = \Gamma(1+1)$ | | |
| 116. | Which is the correct statement for profit ? | | | | | |
| | (A) | Revenue Operating cost | (B) | Revenue Fixed cost | | |
| | (C) | Revenue Total cost | (D) | Revenue Book value | | |
| | | | | | | |
| 117. | The unknown cost of desired capacity can be estimated from the known cost of another | | | | | |
| | 35 35 | pment from the formula | | | | |
| | (A) | $(\cos t)_1 = (\cos t)_2 [(\operatorname{capacity})_2 / (\operatorname{capacity})_2 / (capaci$ | | | | |
| | (B) | $(\cos t)_1 = (\cos t)_2 [(capacity)_1/(capacity)$ | | 6 | | |
| | (C) $(\cos t)_1 = (\cos t)_2 [(\operatorname{capacity})_2 / (\operatorname{capacity})_1]^{0.6}$ | | | | | |
| | (D) $(\cos t)_1 = (\cos t)_2 \left[(\operatorname{capacity})_1 / (\operatorname{capacity})_2 \right]^{0.6}$ | | | | | |
| 118. | For most chemical plants, the ratio of working capital to total capital investment is | | | | | |
| | (A) | 10-20% | (B) | 80-90% | | |
| | (C) | 50-60% | (D) | 1-2% | | |
| 119. | Ditot | tube is used to measure | | | | |
| 117. | | | (B) | point velocity | | |
| | (A) (C) | average velocity volumetric flow rate | (B) (D) | viscosity | | |
| | (C) | volumetric now rate | (D) | viscosity | | |
| 120. | The | cost of heat exchanger is mainly a fo | unctio | n of | | |
| | (A) | Area | (B) | Volume | | |
| | (C) | Orientation | (D) | All of the above | | |
| | | | | | | |
| Set - | A | | 15 | СН | | |
| N 10000 V | | | | | | |

113. The relationship between the effective annual interest rate, i_{eff} and nominal interest rate r is



SPACE FOR ROUGH WORK





CHEMICAL ENGINEERING (CH) SET-A

| Question No | Answer | Question No | Answer |
|-------------|--------|-------------|--------|
| 1 | D | 61 | С |
| 2 | С | 62 | Α |
| 3 | Α | 63 | С |
| 4 | А | 64 | В |
| 5 | Α | 65 | С |
| 6 | С | 66 | В |
| 7 | В | 67 | C |
| 8 | С | 68 | В |
| 9 | Α | 69 | D |
| 10 | D | 70 | Α |
| 11 | С | 71 | С |
| 12 | Α | 72 | В |
| 13 | D | 73 | D |
| 14 | D | 74 | C |
| 15 | В | 75 | Α |
| 16 | Α | 76 | В |
| 17 | D | 77 | C |
| 18 | С | 78 | В |
| 19 | В | 79 | Α |
| 20 | Α | 80 | В |
| 21 | В | 81 | Α |
| 22 | С | 82 | D |
| 23 | Α | 83 | Α |
| 24 | D | 84 | C |
| 25 | Α | 85 | C |
| 26 | В | 86 | D |
| 27 | С | 87 | В |
| 28 | С | 88 | В |
| 29 | В | 89 | C |
| 30 | Α | 90 | В |
| 31 | Α | 91 | В |
| 32 | В | 92 | C |
| 33 | D | 93 | C |
| 34 | Α | 94 | Α |
| 35 | В | 95 | C |
| 36 | Α | 96 | D |
| 37 | D | 97 | В |
| 38 | D | 98 | А |
| 39 | Α | 99 | C |
| 40 | С | 100 | В |



| 41 | В | 101 | D |
|----|---|-----|--------|
| 42 | Α | 102 | C |
| 43 | С | 103 | Α |
| 44 | D | 104 | Α |
| 45 | C | 105 | C |
| 46 | В | 106 | В |
| 47 | C | 107 | D |
| 48 | Α | 108 | В |
| 49 | С | 109 | C |
| 50 | D | 110 | В |
| 51 | В | 111 | Α |
| 52 | С | 112 | C |
| 53 | Α | 113 | В |
| 54 | С | 114 | Α |
| 55 | D | 115 | A C |
| 56 | Α | 116 | C |
| 57 | Α | 117 | D |
| 58 | С | 118 | Α |
| 59 | D | 119 | В |
| 60 | D | 120 | Α |
| | | | |

